

Kongeriget Danmark

Patent application No.: PA 2003 01943

Date of filing: 23 December 2003

Applicant:
(Name and address)
Niro A/S
Gladsaxevej 305
DK-2860 Søborg
Denmark

Title: A method and apparatus for producing micro particles

IPC: -

This is to certify that the attached documents are exact copies of the above mentioned patent application as originally filed.

PRIORITY DOCUMENT
SUBMITTED OR TRANSMITTED IN
COMPLIANCE WITH
RULE 17.1(a) OR (b)

Patent- og Varemærkestyrelsen
Økonomi- og Erhvervsministeriet

22 September 2004

Susanne Morsing
Susanne Morsing



PATENT- OG VAREMÆRKESTYRELSEN



Modtaget

23 DEC. 2003

PVS

1

A method and apparatus for producing micro particles

The invention relates to a method and apparatus for producing substantially monodisperse micro particles, preferably of a heat sensible material or biological active material.

US 4,871,489 A discloses an apparatus and process for producing liquid droplets and solid particles having a narrow size distribution. Thin liquid streams are forced under pressure through a plurality of orifices in an orifice plate, the largest of the orifices having a diameter not greater than about three times the diameter of the smallest of the orifices. The thin liquid streams are oscillated to cause breakup of each stream into droplets having a narrow size distribution. These droplets are subsequently dried to become solid particles having a narrow size distribution. The apparatus and process according to US 4,871,489 is mainly suitable for manufacturing powders of metal oxides. Although powders of metal oxide with excellent characteristics may be produced, the apparatus and process is, however, not suitable for producing powders of heat-sensible material, like e.g. pharmaceutical product. This is due to the fact that exact control of the temperature is difficult in the apparatus and process according to US 4,871,489. Moreover, the disclosed apparatus is constructed in such a way that and efficient cleaning is almost impossible. This, of course, has less significance when dealing with metal oxide powders. However, when dealing with pharmaceutical product, which often has to be handled in sterile environment, it is a major disadvantage.

The object of the present invention is to provide a method and an apparatus for producing micro-particles by spray drying technique of increased uniformity and of increased density in relation to traditionally spray dried particles, and preferably particles of heat-sensible material, in particular micro-particles of heat-sensible pharmaceutical materials. The increased uniformity means that the particles are substantially monodisperse, i.e. with a very narrow span.

With a view to this the present invention relates in a first aspect to a method for producing micro particles, preferably of a heat sensible material, which method comprises at least the steps of:

- 15 - feeding a feed material to an orifice, said feed material comprising a solution or dispersion or suspension of the heat sensible material,
 - 20 - ejecting the feed material from the orifice as micro spheres having substantially the same mean particle size,
 - 25 - subjecting the micro spheres ejected from the orifice to a stream of a carrier gas carrying the micro spheres onwards into a drying chamber, and
 - 30 - subjecting the micro spheres to a drying gas causing evaporation of the volatile liquid and drying of the micro spheres into solid particles in the drying gas in the drying chamber,
- characterized in that the temperature of the carrier

gas in the area in front of the orifice is lower than the temperature of the drying gas in the drying chamber.

The relatively cold stream of carrier gas 5 serves to fetch the micro particles ejected from the orifice and carry them onwards into the warmer drying gas wherein the micro particles are gently heated to a temperature allowing gradually more intense evaporation of the volatile liquid as the carrier gas is 10 intermixed with the drying gas. Simultaneously with the heating caused by the increasing amount of heating gas in the mixture of carrier gas, particles and heating gas, the particles are distributed over the drying chamber so that a large quantity of drying gas 15 is available to every particle. This distribution is important for the possibilities of effecting a gentle drying of the particles in the chamber, and in addition the risk of agglomeration of particles is reduced to a minimum. The latter effect ensures that 20 the resulting dried particles have the so-called monodisperse size distribution, that is particles having very even particle size. The combined effects of the invention result in particles of a very dense structure.

25 The feed material enters the drying chamber as micro spheres via the orifice, which breaks the stream of liquid feed material into substantially uniform micro spheres. The orifice may be part of a nozzle. In the drying chamber the micro spheres are 30 almost instantly brought into contact with the carrier gas, having a relatively low temperature in relation to the temperature present in the actual drying chamber. Depending on the characteristics of the

volatile liquid some initial drying or removal of volatile liquid from the micro spheres can possibly take place in the upper portion of the drying chamber. Subsequently the micro spheres are brought into contact with the drying gas having higher temperature than the carrier gas. The drying gas gradually removes substantially all of the remaining volatile liquid from the micro spheres and transforms them into solid micro particles before they drop out of the drying liquid in the end of the drying chamber. Preferably less than 9%, more preferred less than 6% by weight of residual volatiles are left in the formed micro particles.

The volatile liquid may be any liquid suitable for serving as volatile liquid for the heat-sensible material, e.g. water, alcohol, ether, acetone etc.

The temperature of the drying gas should be selected to be well below the temperature where the heat-sensible material starts to decompose or transform to secure that the heat-sensible material keeps its desired properties in the micro particles. Preferably, the temperature of the drying gas is at least 5-10°C below the temperature where the heat-sensible material starts to decompose or transform, more preferred at least 10-20°C below this temperature.

The amount of the carrier gas led to the drying chamber is typically much lower than the amount of the drying gas led to the drying chamber. Preferably the amount of carrier gas constitutes 1-10% by weight in relation to the drying gas. The carrier gas may for some purposes be a saturated gas. A saturated gas has no ability of drying, but can to the contrary cool the micro spheres.

The method according to the invention produces micro particles of heat sensible material having excellent properties. The desired activity and properties of the heat sensible material can be maintained over extended time when the heat sensible material is processed by the method according to the invention. The micro particles according to the invention have mean particle sizes within a narrow range and are very dense. The pore volume constitutes only a minor part of the total volume of the micro particles. These properties are very advantageous, in particular when the heat sensible material is a pharmaceutical intended for use in needleless syringes.

The apparatus according to the invention is easy to operate and clean. The apparatus can be cleaned to obtain sterile conditions and it is in particular possible to apply CIP procedures (Cleaning In Place) for easy operation of the apparatus.

Moreover, the construction of the apparatus according to the invention has the unexpected advantageously effect that the drying volume of the apparatus can be surprisingly small. This reduces the cost for manufacture, and space required.

After drying by the method of the invention in the drying chamber, the micro particles may optionally be subjected to a separation step e.g. in a cyclone. However, such particle/gas separation processes are well-known to the skilled person and need not to be described in further details.

Although the temperatures of the carrier gas and the drying gas can be selected rather freely as long they meet the criteria for drying gas as stated above, it is preferred that the inlet temperature of

the carrier gas is in the range below 40°C, more preferred in a range below 25°C. The inlet temperature of the carrier gas should not be lower than the freezing point of the volatile liquid used. Preferably the 5 inlet temperature of the drying gas is in the range from 30 to 120°C, more preferred in the range from 40 to 80°C. These preferred temperature intervals fulfil the requirements of a large range of heat-sensible materials used within the pharmaceutical industry, 10 and are also well suited for other heat sensible materials.

In a preferred embodiment of the method according to the invention the micro spheres and the carrier gas is introduced into an area in the upper part 15 of the drying chamber, and the drying gas is introduced into the drying chamber in an area below the area where the carrier gas is introduced. In this manner a very gentle, but yet efficient, removal of volatile liquid from the micro spheres is obtained, 20 and the micro spheres are allowed to flow some distance into the drying chamber before being surrounded by drying gas, because the inflowing drying gas does not disturb the flow of carrier gas in vicinity of the orifice. This allows the carrier gas to 25 get a safe hold of the micro spheres when they are ejected from the orifice, so that the micro spheres are carried well into the drying chamber before heating takes place.

Although the carrier gas may serve to remove 30 some part of the volatile liquid from the micro spheres the carrier gas primarily serves simply to disperse the micro spheres into the drying gas in or-

der to improve the above mentioned gentle drying and keeping the feeding orifice cool.

It is preferred that the carrier gas flows about the orifice in a swirling spiral motion, which 5 improves the separation of the carrier gas from the drying gas in the upper portion of the drying chamber so that the micro spheres are carried deeper into the drying chamber before being heated by the drying gas. The micro spheres are consequently more finely dispersed in the chamber, and the drying becomes more even among all micro spheres, and the resulting product obtains better and more well defined product properties.

For the purpose of obtaining a highly efficient 15 dispersion of the micro spheres into the drying gas the carrier gas can in its swirling spiral motion flow with a swirl number > 1 , and more preferred with a swirl number > 2 . The swirl number specifies the level of swirl in a spiral or vortex motion. The 20 swirl number S is defined in terms of the ratio of the angular momentum flux, M_{ang} , to the axial momentum flux, M_{ax} , at a given cross section, so that for incompressible flow $S = M_{ang}/aM_{ax}$, where a is the outer radius of the vortex flow (for further details, see: 25 Internal fluid flow; The fluid dynamics of flow in pipes and ducts; A. J. Ward-Smith; Clarendon Press, Oxford 1980, in particular chapter K "Flows with swirl").

The flow of drying gas in prior art drying 30 chambers is typically turbulent. However, in the method according to the invention it is preferred that the flow of the drying gas includes a substantially laminar flow coaxially in the drying chamber.

8

The laminar flow has low velocity, typically < 0,5 m/s, preferably < 0,3 m/s. A substantially laminar flow along the side walls also of the drying chamber serves to prevent sticking of heat-sensible material 5 to the side wall, because the laminar flow is separate from the tubular flow and difficult to enter for particles because of its stability as a boundary layer near the side wall. The laminar flow at the side walls increases the yield of heat-sensible material 10 from the drying chamber.

In principle the micro spheres can be generated in any known manner, but preferably the method includes a oscillating device that acts on the feed and/or on the feed device having the orifice located 15 at its delivery end. The delivery end is placed in the drying chamber, preferably in the upper and/or top part of the drying chamber above the drying gas inlet.

The oscillating device can be a mechanical, 20 sonic or magnetic oscillating device, and preferably the oscillating device includes one or more piezo electric crystals. Piezo electric crystals are capable of oscillating with a very precise frequency, thus enhancing the uniformity of the size of the 25 micro spheres. Piezo electric crystal can moreover oscillate with very high frequencies, which is very advantageously for the purpose of forming small micro spheres.

In a preferred embodiment of the method according 30 to the invention the carrier gas flows into the drying chamber in a spiral motion encircling the delivery end of the feed device. Thereby the carrier gas catches the formed micro spheres in the flow that

penetrates well into the drying chamber. The spiral flow is in itself less turbulent and more even which acts to prevent that the micro spheres collide and merge. A merging of the micro spheres is highly undesired as it will lead to particles with different sizes and consequently the uniformity of the particles cannot be well controlled. Furthermore, according to the method of the invention the flow of carrier gas is adapted so it has no atomising effect on 10 the micro spheres. An atomising effect will also lead to a situation where the uniformity of the formed particles cannot be controlled.

Although all gasses that are inert to the heat-sensitive material are suitable for use in the method 15 according to the invention it is preferred that the carrier gas and the drying gas are selected from atmospheric air, nitrogen, argon, helium, carbondioxide, and mixtures thereof and optionally sterilised. The carrier gas and the drying gas may be the same or 20 different. Air is suitable as drying gas for many non-water solvents due to the large amount of drying gas used in relation to the amount of non-water volatiles in the drying gas. Thus, the risk of explosions is eliminated.

25 According to the method the yield of heat sensible material is higher than 90%, preferably higher than 95%, of the theoretical yield. The theoretical yield is a yield where 100% of the heat-sensitive material led to the drying chamber in solution or dispersion is present in the recovered micro particles, or in other words there is no loss of material in the process line equipment. Thus, the invention provides 30 for very high yields and very little loss of the

heat-sensible material. This is advantageously, in particular when the heat-sensible material is expensive or involves active substances that cannot be released to the environment.

5 In a second aspect the present invention relates to an apparatus producing dried micro particles with a high density. The particles are preferably of a heat sensible material. The apparatus comprises a drying chamber having at least one inlet for a drying 10 gas, and at least one feed device with an orifice for ejecting micro spheres, and it is characterized in that the feed device is an elongate member with a feeding end for receiving feeding material and a delivery end with an orifice for ejecting micro spheres 15 of feeding material, that the feed device is surrounded by an elongate outer tube with an air gap between an outer surface of the feed device and an inner surface of the tube, that the tube has a longitudinal axis and at least one inlet for carrier gas ar- 20 ranged tangential to the longitudinal axis at a position in between the feeding end and the delivery end of the feed device.

The outer tube and the air gap directs the carrier gas in a flow that not only provides a flow envelope 25 of carrier gas around the feed device, but also make the carrier gas entrap the micro spheres and penetrate a distance into the drying chamber together with the particles substantially without any intermixing of drying air into the flow. Due to the tan- 30 gential inlet of the carrier gas to the air gap the carrier gas will flow in a rotation motion onwards through the air gap and past the orifice into the drying chamber. The carrier gas is thus effecting a

11

swirling movement that keeps the carrier gas separate from the drying gas until the area inside the drying chamber where the swirling movement looses its momentum and the flow of carrier gas with the micro spheres is dissolved in the drying gas with consequent intermixing of the gasses and gradual heating of the micro spheres due to the higher temperature of the drying gas. At the time when the micro spheres are heated due to intermixing of drying gas, the micro spheres are also distributed over the cross-sectional area of the drying chamber. The resulting dispersion of the micro spheres in the drying gas is so even that substantially all micro spheres are subjected to the same, gentle drying conditions. Due to the fact that the drying only sets in gradually, the micro spheres are dried to very dense particles.

The feed device preferably includes a oscillation device capable of generating mutual oscillation between the feeding material and the feeding end of the feed device. The oscillation assists in breaking up the liquid feed into uniformly sized micro spheres. Adjustment of the frequency of oscillation can, together with the pressure of the liquid fee, be utilized to adjust the size of the micro spheres. The oscillation device can act mechanically on the feed device to cause it to oscillate or can act on the feed material via a member located in contact with the liquid feed material, or the oscillation device can interact with the fluid to cause non-mechanical pressure variations in the liquid.

Preferably, the oscillation device includes oscillating means in the form of one or more piezo electric crystals, which can be joined to the outer sur-

face of the elongate member. The piezo electric crystals have the advantage of being simple to control via an electric source.

In the most preferred embodiment the feed device 5 in the tube is mounted in an upper end wall of the drying chamber with the longitudinal axis of the tube extending in parallel with a longitudinal axis of the drying chamber, preferably coaxially therewith. This entails several advantages. With this orientation of 10 the feed device the flow of carrier gas is directed in the longitudinal direction of the drying chamber, because the annular air gap between the elongate member and the tube provides the carrier gas with a distinct flow direction, and the mounting of the feed 15 device in the upper end wall of the drying chamber makes the micro spheres flow downwards assisted by the effect of gravity which promotes a uniform flow down through the drying chamber.

Although it is possible to locate the at least 20 one inlet for drying gas above or equal to the level of the orifice at the delivery end of the elongate member it is, however, preferred that the at least one inlet for drying gas is located at a level below the orifice at the delivery end of the elongate mem- 25 ber. The embodiment secures that a very gentle, but yet efficient, removal of volatile liquid from the micro spheres is obtained. The micro spheres can flow some distance into the drying chamber before they meet the drying gas, because the inflowing drying gas 30 does not disturb the flow of carrier gas in vicinity of the orifice. This allows the carrier gas to get a safe hold of the micro spheres when they are ejected from the orifice, so that the micro spheres are car-

DEC. 23 '2003 18:28 +004543999902

13

ried well into the drying chamber before heating takes place.

In a preferred embodiment of the apparatus according to the invention the apparatus comprises a plurality of feed devices for generating micro spheres. Preferably the apparatus comprises 2 to 8 feed devices arranged in the upper end wall of the drying chamber. The plurality of feed devices increases the capacity of the dryer.

10 In preferred embodiments of the apparatus according to the invention the volume of the drying chamber is less than 0.1 m^3 , and preferably larger than 0.03 m^3 , when the produced particles have an mean particle size in the range of $1\text{-}59 \mu\text{m}$ and the volume of the 15 drying chamber is less than 0.3 m^3 , and preferably larger than 0.1 m^3 , when the produced particles have an mean particle size in the range of $60\text{-}120 \mu\text{m}$. These relations between the volume of the drying chamber and the mean particle size of the produced 20 particles have proven to give optimal conditions for drying the micro spheres into particles with uniform size that have higher density than traditional spray dried particles.

Preferably the at least one inlet for carrier gas 25 is connected to a gas supply device providing an inflow of carrier gas to the air gap resulting in swirling motion of the carrier gas in the air gap with a swirl number $> 0,5$. An inflow of carrier gas to the air gap resulting in a swirl number $> 0,5$ for 30 the carrier gas serves to facilitate the dispersion of the micro spheres into the drying gas and prevent the micro spheres in colliding. Preferably the swirl number is > 1 to improve the effect, more preferably

the swirl number is > 2 to obtain an even better effect.

In the apparatus according to the invention it is preferred that the length of the drying chamber is at least 3.5 times longer than the diameter of the drying chamber. The length of the drying chamber substantially determines the residence time of the micro spheres in the drying chamber and as a consequence the level of drying. An optimal length for efficient 10 drying has proven to be at least 3.5 times longer than the diameter of the drying chamber.

Preferably the inlet for drying gas is provided with a filter substantially sterilizing the drying gas, thereby achieving a substantially sterile environment in the drying chamber, which is highly advantageously when drying pharmaceuticals.

Examples of the invention are in the following described in further details with reference to the very schematic drawings, on which:

20

Fig. 1 illustrates an embodiment of the apparatus according to the invention,

25

Fig. 2 depicts an enlarged longitudinal section through a nozzle device of the apparatus in Fig. 1,

30

Fig. 3 depicts a horizontal section through the nozzle device of Fig. 2, along the line A-A,

Fig. 4 illustrates an embodiment of the apparatus according to the invention with more nozzle devices in the upper plate,

Fig. 5 shows an alternative embodiment of the

15

apparatus according to the invention,
and

Fig. 6 shows micro particles produced accord-
ing to the invention.

5

The term "micro spheres" refers to substantially spherically droplets optionally including heat-sensible material in a volatile liquid. The droplets have mean particle sizes within the range 10 from about 1 to about 120 μm .

As used herein the term "micro particles" refers to small particles, which are substantially spherically and have mean particle sizes within the range from about 1 to about 120 μm .

15 The term "mean particle size" as used herein is defined as the volume of a sphere having the D_{50} diameter. Thus, particles having the same volume as said sphere have the same mean particle size, although they may not be spherically.

20 The term "span" is defined as $(D_{90} - D_{10})/D_{50}$ in which D_{10} , D_{50} and D_{90} denotes the diameters of the 10% fractile, the 50% fractile and the 90% fractile, respectively.

25 The term "heat-sensible material" refers to a material, which includes at least one constituent that will decompose or transform when subjected to heat or a temperature above a certain level. The typical level for temperatures that are harmful to heat-sensible material is a temperature above 60 - 30 140°C. Common heat-sensible materials include biological materials and pharmaceutical material. In this context the term heat-sensible material also includes biological active material, which is only lesser

heat-sensible.

As used herein "drying gas" means any gaseous medium capable of receiving and transporting evaporated volatile liquid.

5 The term "volatile liquid" as used herein, refers to any liquid medium suitable for dissolving the heat-sensible material or forming a stable dispersion or suspension with the heat-sensible material and being able of evaporating from said solution, dispersion or suspension.

Figure 1 depicts an apparatus according to the invention. The apparatus comprises a drying chamber 1, having a cylindrical upper part 2 and a conical bottom part 3. The cylindrical upper part 2 is 15 equipped with a heating mantle 4. The top of the drying chamber 1 is closed with an upper wall 5. The upper wall includes a device 6 for generating micro spheres and inlet 7 for a carrier gas. The upper part includes furthermore an inlet 8 for a drying gas. The 20 inlet 8 is equipped with filters 9 to filtrate the drying gas and produce a diffuse flow of drying gas. The generated particles and used drying gas leaves through outlet 10 in the bottom part 3 of the drying chamber 1.

25 During operation, the heat-sensible material enters the drying chamber 1 included in micro spheres via an orifice in the device 6. The carrier gas enters the drying chamber via inlet 7, which encircle the orifice in the device 6 to facilitate immediate 30 contact between the micro spheres and the carrier gas to initiate a dispersion of the micro spheres into the drying gas, which enters the drying chamber 1 via inlet 8. The filters 9 causes a diffuse flow of dry-

ing gas into the drying chamber 1, which will facilitate formation of substantially laminar flow of drying gas in the drying chamber 1. In principal the filters can be any filter device with any desired shape as long as they are able to facilitate the formation of a substantially laminar flow in the reactor. The micro spheres passes towards the bottom part 3 through the cylindrical part 2 of the drying chamber 1. During the passage the micro spheres give off substantially all volatile liquid to the drying gas. When they reach the outlet 10 in the conical bottom part 3 they have been transformed into micro particles.

Figure 2 illustrates a preferred embodiment of 15 a nozzle 11 according to the invention. The nozzle is suitable as device 6 for generating micro spheres and inlet for carrier gas as shown in figure 1. With reference to figure 2 the nozzle 11 comprises an inner tube 12 with a feeding end 13 and a delivery end 14. 20 The delivery end 14 is tapered with an orifice 14a at the tapered end. The feeding end 13 receives feed 15 and the orifice 14a at the delivery end 14 delivers micro spheres 16. The inner tube 12 is in contact with piezo electric crystals connected to a source 25 for electric voltage 18 via wires 18a. The inner tube 12 is encircled in an outer tube 19 thereby forming an annular gap 20 between the inner tube 12 and the outer tube 19. Moreover, the gap 20 is connected to an inlet 21 for carrier gas 22. The inner tube 12 and 30 the outer tube 19 forms an annular outlet 23 for carrier gas encircling the delivery end 14.

As seen in figure 3, which depict the cross section in respect of the line A-A in figure 2 the

inlet 21 is arranged tangentially into the gab 19 thereby promoting a swirling motion of the carrier gas from the annular outlet 23.

During operation the material to be formed into micro particles is feed to the feeding end 13 of the tube 12 as a solution or dispersion in a volatile liquid 15. In the tube 12 the feed 15 is subjected to oscillations from the piezo electric crystals 17 and when the feed 15 leaves the tube via orifice 14a in 10 the delivery end 14 it instantly breaks into micro spheres 16 of substantially uniform size.

Simultaneously a flow of carrier gas is led to the annular outlet 23 via inlet 21 and gab 19. Due to tangentially arrangement of inlet 21 into gab 19 the carrier gas will obtain a flow with spiral movement, which will remain a while after the drying gas is released from annular outlet 23, and engage with the micro spheres. Thereby is obtained a dispersing effect on the micro spheres 16 in combination with a 20 cooling flow of gas over the tube 12 and the delivery end 14.

Figure 4 shows an embodiment of the apparatus according to the invention with more devices for generating micro spheres and inlets for carrier gas. Using the same reference numbers for the same parts as in figure 1 the apparatus includes a drying chamber 1 in a cylindrical part 2 and conical bottom part 3. The cylindrical part is equipped with a heating mantel 4 for temperature control. The upper wall 5 comprises more devices 6a, 6b, 6c, 6d for generating micro spheres and inlets 7a, 7b, 7c, 7d. In principal the dryer may comprise numerous of devices for generating micro spheres arranged in an array. Moreover,

the apparatus includes an inlet 8 for drying gasses including filters 9 for filtering the drying gas. The embodiment provides for an apparatus, which can produce micro particles with increased yield.

5 Figure 5 depict yet an alternative embodiment of the apparatus according to the invention. For the reason of clarity the same reference numbers for the same parts as in figure 1 are used. Thus, the apparatus includes a drying chamber 1 in a cylindrical part 10 2 and conical bottom part 3. The cylindrical part is equipped with a heating mantel 4 for temperature control. The upper wall 5 comprises a device 6 for generating micro spheres and an inlet 7 for carrier gas. Below the upper wall 5 is the inlet 8 for drying gas 15 located. Additional the apparatus is equipped with an outlet device 20 for micro particles and spent carrier- and drying gas. The mixture of micro particles and spent carrier- and drying gas is lead to particle/gas separator 21, where the particles are taken 20 of at 22. The gas is via pipe 23 led to regenerating device 24 to be recycled to the drying chamber 1. From the regenerating device 24 a first stream 25 is recycled to the drying chamber 1 as carrier gas by 25 use of pump 27 and passing the cooler 26 to cool the carrier gas. A second stream 28 is recycled to the drying chamber 1 as drying gas after being heated in heater 29. This embodiment closed cycle is particular suitable, in particular when the heat-sensible material is expensive or involves active substances that 30 cannot be released to the environment and/or the gas used is inert.

The cross section of drying chamber may have any desired shape, circular, oval, square etc., the

20

preferred shape of the cross section is circular.

The method and apparatus according to the invention produces micro particles having a very uniform size, typically with a span < 0,5. Moreover, the 5 micro particles have a significant higher density (less porosity) than the micro particles manufactured in traditional spray dryers. Further, it is possible to produce larger particles compared to prior art spray drying equipment of similar dimensions.

10

EXAMPLE

The method according to the invention was tested on a sample of heat-sensible material using an 15 apparatus according to the invention and in principle as described above.

The test sample consisted of trehalose, OVA (egg albinum) and β -galactosidase with the composition as described in table 1

20

Table 1. Composition of test sample

| Compound | amount in % by weight |
|------------------------|-----------------------|
| Trehalose | 90 |
| OVA (egg albinum) | 5 |
| β -galactosidase | 5 |

β -galactosidase is a heat-sensible enzyme and consequently suitable for testing the method and ap-25 paratus according to the invention.

The apparatus comprised a cylindrical drying chamber with the approx dimensions: height 100 cm, diameter 25 cm. The volume of the drying chamber was

21

approx. 0,05 m³. Moreover the apparatus were equipped with a nozzle according to the invention with an inner tube with approx diameter 5 mm, tapered in the delivery end to have an substantially circular outlet orifice with a diameter of approx 25 µm. The inner tube had a piezo electric plate placed on the outer surface. The piezo electric plate was operated with a frequency of 40000 Hz. The outer tube had a diameter of approx 8 mm.

During the test the sample was feed to the drying chamber via the orifice as 24 % weight solution in water under the conditions shown in table 2. The amount of solid material used in the test was 30 g.

15 Table 2. Operation conditions

| | |
|--------------------------|-----------|
| Inlet temperature | 72°C |
| Outlet temperature | 70°C |
| Carrier gas rate | 1 kg/h |
| Carrier gas temperature | 20°C |
| Drying gas rate | 25 kg/h |
| Residence time | 7 sec |
| Particle diameter | 42 micron |
| Feed rate | 28 g/h |
| Feed pressure | 1.1 bar |
| Orifice diameter | 25 micron |
| Frequency of piezo plate | 40000 Hz |

Substantially uniform micro particles were produced. The micro particles obtained were substantially spherically with a diameter of approx 42 µm. Test material was present in the particles in a recovered amount of > 98 % of the material in the feed

22

(i.e. yield > 98%). The produced particles had a residual moisture of 4.9 %, and the enzymatic activity of the heat-sensible material was fully maintained. Carrier gas and drying gas was filtered atmospheric
5 air.

A reflective light photography of the produced particles are shown in figure 6, from which it can be seen that the particles are substantially uniform and spherically.

10

15

23

P A T E N T C L A I M S

1. A method for producing substantially monodisperse micro particles, preferably of a heat sensible material, said method comprising at least the steps 5 of:

- feeding a feed material to an orifice, said feed material comprising a solution or dispersion or suspension of the heat sensible material.
- 10 ejecting the feed material from the orifice as micro spheres having diameters of substantially the same size.
- 15 subjecting the micro spheres ejected from the orifice to a stream of a carrier gas carrying the micro spheres onwards into a drying chamber, and
- 20 subjecting the micro spheres to a drying gas causing evaporation of the volatile liquid and drying of the micro spheres into solid particles in the drying gas in the drying chamber, characterized in that the temperature of the carrier gas in the area in front of the orifice is lower than the temperature of the drying gas 25 in the drying chamber.

2. A method according to claim 1, wherein the inlet temperature of the carrier gas is in a range below 40°C, preferably in a range below 25°C.

3. A method according to claim 1 or 2, wherein the 30 inlet temperature of the drying gas is in the range from 30 to 120°C, preferably in the range from 40 to 80°C.

24

4. A method according to any one of claims 1 to 3, wherein the second dryings gas is introduced into the drying chamber at an area below the area where the carrier gas is introduced.
5. A method according to any one of claims 1 to 4, wherein the carrier gas disperses the generated micro spheres into the drying gas.
6. A method according to any one of claims 1 to 5, wherein the carrier gas flows about the orifice in a swirling motion.
7. A method according to claim 6, wherein the carrier gas in its swirling motion flows with a swirl number > 0,5, and preferably with a swirl number > 1, more preferably with a swirl number > 2.
- 15 8. A method according to any one of claims 1 to 7, wherein the flow of said drying gas includes a substantially laminar flow in the drying chamber.
9. A method according to claim 8 wherein the velocity of the substantially laminar flow is < 0,5 m/s, preferably < 0,3 m/s.
10. A method according to any one of claims 1 to 9, wherein a oscillating device acts on the feed and/or on a feed device having said orifice located at a delivery end.
- 25 11. A method according to claim 10, wherein the oscillating device includes one or more piezo electric crystals.
12. A method according to claim 10 or 11, wherein the carrier gas flows into the drying chamber in a swirling motion encircling the delivery end of the feed device.
13. A method according to any one of claims 1 to 12, wherein the carrier gas and the drying gas are

selected from atmospheric air, nitrogen, argon, helium, carbondioxide, optionally sterilised and mixtures thereof.

14. A method according to any one of the claims 1 to 13, wherein the carrier gas is a saturated gas.

15. A method according to any one of claims 1 to 14, wherein the yield of heat sensible material is higher than 90%, preferably higher than 95% of the theoretical yield.

10 16. A method according to any one of the claims 1 to 15, wherein the particles have a mean particle size with a span < 0,5.

17. An apparatus producing substantially monodisperse micro particles, preferably of a heat sensible material, and comprising a drying chamber having at least one inlet for a drying gas, and at least one feed device with an orifice for ejecting micro spheres, characterized in that the feed device has a feeding end for receiving feeding material and a delivery end with an orifice for ejecting micro spheres of feeding material, that the feed device is surrounded by an outer tube with an air gap between an outer surface of the feed device and an inner surface of the tube, that the tube has a longitudinal axis and at least one inlet for carrier gas arranged tangential to the longitudinal axis at a position in between the feeding end and the delivery end of the feed device.

18. An apparatus according to claim 17, characterized in that the feed device includes a oscillation device capable of generating mutual oscillation between the feeding material and the feeding end of the feed device.

19. An apparatus according to claim 17 or 18, characterized in that the oscillation device includes oscillating means in the form of one or more piezo electric crystals.

5 20. An apparatus according to any one of claims 17 to 19, characterized in that the feed device in the tube is mounted in an upper end wall of the drying chamber with the longitudinal axis of the tube extending in parallel with a longitudinal axis 10 of the drying chamber, preferably coaxially therewith.

21. An apparatus according to claim 20, characterized in that the at least one inlet for drying gas is located at a level below the 15 orifice at the delivery end of the elongate member.

22. An apparatus according to any one of claims 17 to 21, characterized in that the apparatus comprises a plurality of feed devices for generating micro spheres, preferably 2 to 8 feed devices 20 arranged in the upper end wall of the drying chamber.

23. An apparatus according to claims 21 or 22, characterized in that the diameter of the drying chamber is increased at a level below the inlet for drying gas.

25 24. An apparatus according to any one of claims 17 to 23, characterized in that the volume of the drying chamber is less than 0.10 m³, and preferably larger than 0.03 m³, when the produced particles have a mean particle size in the range of 1-59 30 μm.

25. An apparatus according to any one of claims 17 to 23, characterized in that the volume of the drying chamber is less than 0.30 m³, and pref-

27

erably larger than 0.1 m^3 , when the produced particles have an mean particle size in the range of $60\text{-}120 \mu\text{m}$.

26. An apparatus according to any one of claims 17 to 25, characterized in that the at least one inlet for carrier gas is connected to a gas supply device providing an inflow of carrier gas to the air gap resulting in swirling motion of the carrier gas in the air gap with a swirl number $> 0,5$, preferably a swirl number > 1 , more preferably a swirl number > 2 .

27. An apparatus according to any one of claims 17 to 26, characterized in that the length of the drying chamber is at least 3.5 times longer than the diameter of the drying chamber.

15 28. An apparatus according to any one of claims 17 to 27, characterized in that the inlet for drying gas is provided with a filter substantially sterilizing the drying gas.

20

A B S T R A C T

A method and apparatus for producing micro particles

5

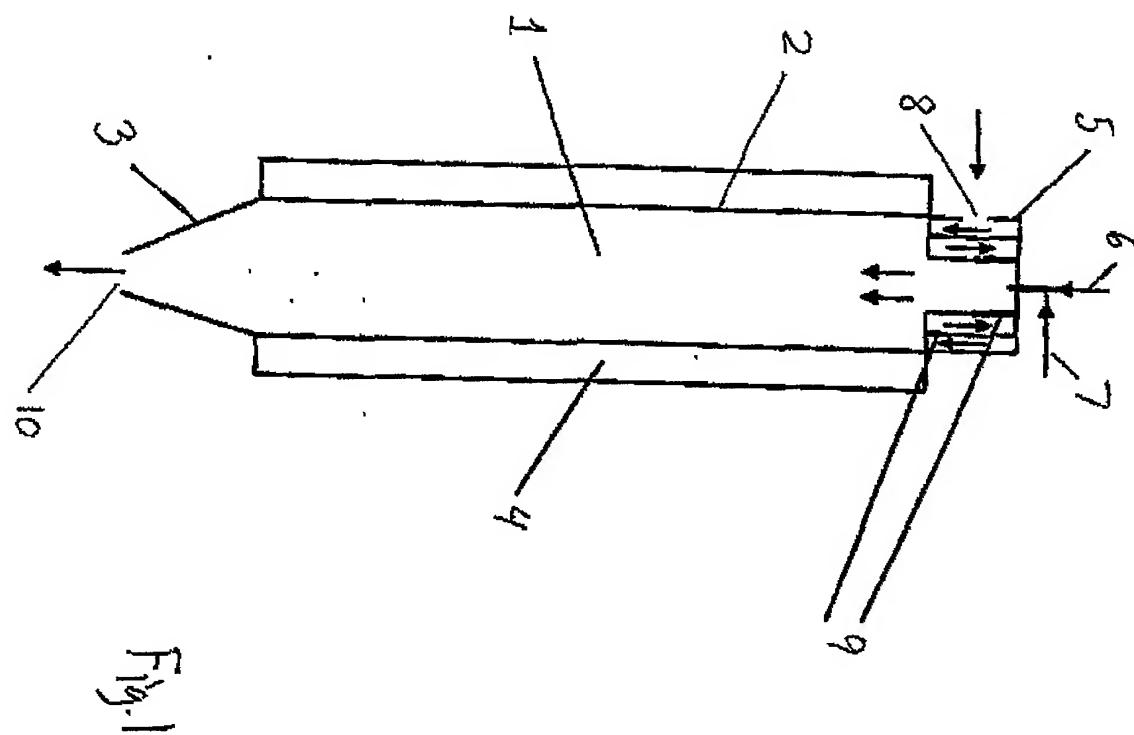
The invention relates to a method and apparatus for producing substantially monodisperse micro particles preferably of heat sensible material using a carrier gas and a drying gas. Relatively dense micro particles with diameters in the range 1-120 μm with a very narrow span can be obtained.

(Fig.1)

Modtaget

23 DEC. 2003

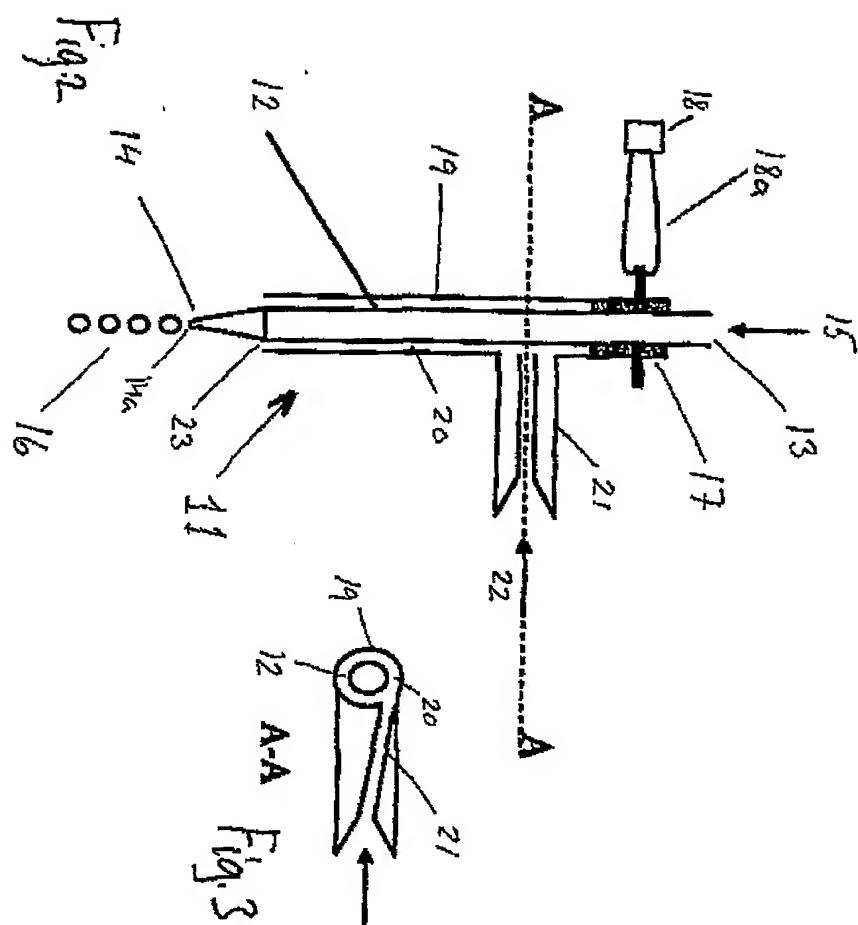
PVS



Modtaget

23 DEC. 2003

PVS



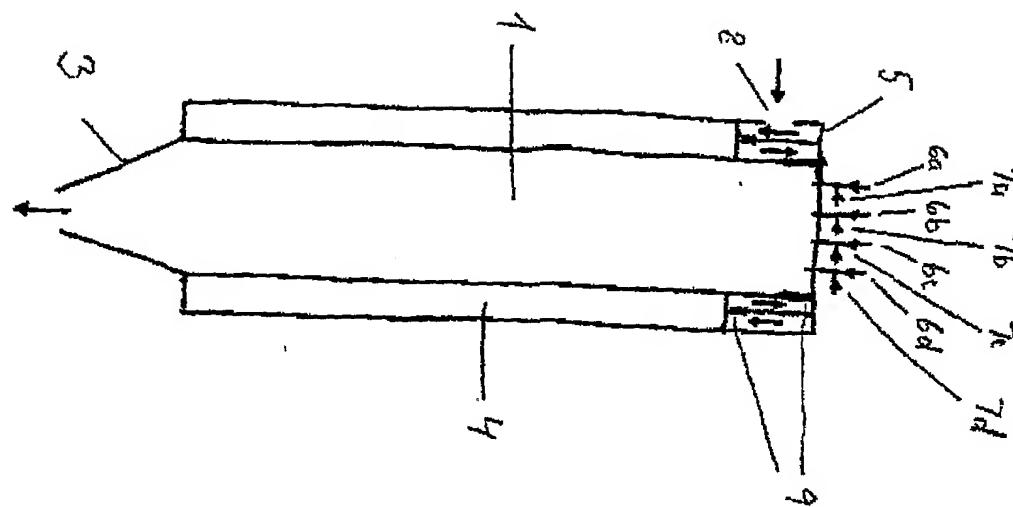
Modtaget

23 DEC. 2003

PVS

Fig

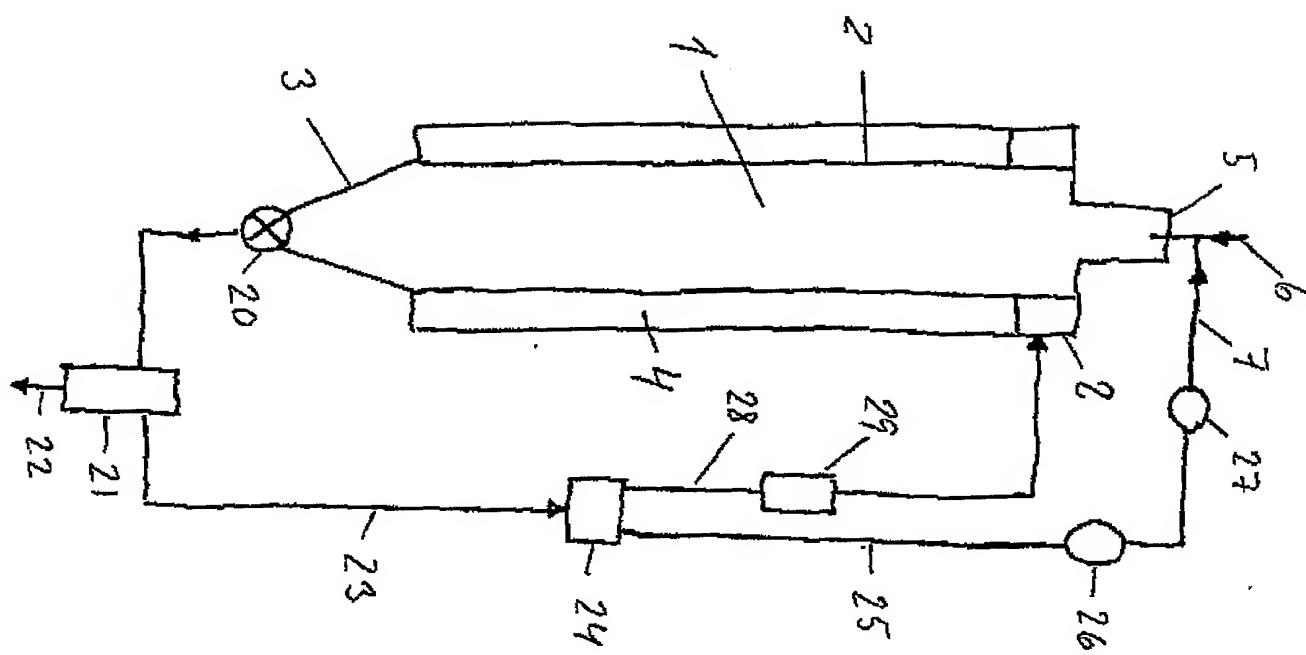
4



Modtaget

23 DEC. 2003

PVS

Fig
5

DEC. 23 2003 10:30 +004543999902

INTERNATIONAL PATENT BUREAU

#3583 P.035/035

D.D.

Modtaget

23 DEC. 2003

PVS

Fig. 6 Uniform trehalose-OVA- β -galactosidase particles in reflected light viewing.

